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MHD Casson flow of a Rotating liquid past a porous medium in the presence of Thermal Radiation and Chemical Reaction

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ABSTRACT: Soret and Dufour effects have a major impact on flows involving temperature and concentration gradients. To give just one example, the Soret effect has been employed in the process of blending gases that have various molecular weights and in the process of discriminating between isotope pairings respectively. In this work, the laminar Casson flow of a fluid rotating across a permeable plate undergoing a chemical reaction is the subject of investigation. The essay emphasizes investigating how radiation, Soret, and Dufour influence the flow of the fluid. Due to the use of similarity variables, the governing equations and the accompanying boundary conditions are reduced to a dimensionless form. Subsequently, the equations are solved by ND with the assistance of the MATHEMATICA program. By using the flow's dimensionless properties, we were able to derive numerical estimates of temperature, concentration, and velocity. The images that were produced because of this process were exhibited. Higher Soret and Dufour parameters, in conjunction with a rise in the radiation factor, led to improved velocity profiles and warm temperature distribution. These are the most important findings that were uncovered as a result of the investigation.

Key Words: Soret and Dufour effect; laminar flow; thermal radiation; porous media.

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1. Introduction

Thermal radiation in fluid dynamics is crucial in multiple fields of engineering, including aeronautical, solar power, chemical, environmental, and mechanical. Controlling heat is essential for preserving operational effectiveness and avoiding overheating in electronic equipment, industrial processes, and power plants. Engineers who are knowledgeable about radiative heat transfer may create efficient cooling solutions like heat sinks and radiative shields. Heat and mass transport in a liquid with varying viscosity via a penetrable upright plate subject to a magnetic field was considered through Makinde and Ogulu [1] and their findings indicate that an upsurge in the viscosity will reduce the velocity profiles and greater estimations of radiation factor will increase the temperature distribution. In the presence of a power-law velocity [2,3], MHD flow with heat transfer across a stretched surface was postulated by Anjali Devi and David [4]. Sulochana et al. [5] explored the mass & heat transport behavior of magnetized flow across a vertically rotating cone in a permeable media subject to chemical reaction, Soret effects, and thermal radiation and results showed that varying the porosity parameter improved heat and mass transport. Multiple models have been used in recent research in this field [6,7,8,9,10,12].

Rotating porous media refers to a type of material or medium that has a porous structure and is capable of rotation. When pores are present, fluids or gases may pass through the material, and rotation adds another dynamic component. Rotation and porosity work together to provide a variety of intriguing phenomena and applications in a wide range of industries. A few instances of rotating porous medium are separation and filtering filtration, and separation procedures may be carried out using a rotating porous medium [13]. The medium may successfully separate suspended particles or separate various components

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of a mixture depending on their density or size by applying centrifugal forces as a result of rotation. This is very helpful for the chemical processing, oil and gas sector, and wastewater treatment. Rotating porous media may improve the processes of heat and mass transmission [14]. Rotating porous media, for instance, may increase the thermal convective coefficient and decrease boundary layer heaviness to enhance the thermal efficiency in heat exchangers. This has uses in cooling devices, HVAC (ventilation, heating, and air conditioning) systems, and electronic device thermal management. Rotating porous media may be used in biomedical applications such as tissue engineering, bio-filtration, and drug delivery systems [15]. The development and survival of cells and tissues may be aided by the controlled rotation of porous scaffolds by improving nutrition and oxygen delivery. Additionally, it may aid in waste elimination and boost the effectiveness of medicine administration. Anika et al. [16] conducted an experiment to examine the effect of Hall current on MHD fluid flow across an endlessly rotating vertical plate with heat transfer. They found that increasing the rotation parameter reduced the velocity profiles. Hayat and Hutter [17] examined the behavior of a second-order incompressible rotating flow past a porous plate and their research reveals that the velocity field exhibits a non-Newtonian influence in both the steady and the unsteady states. The magnetohydrodynamic (MHD) flow of an elastic viscous fluid through a permeable media is affected by Hall and ion slip effects. Krishna and Chamka's [18] computer analysis revealed that both elasticity and the magnetic field impede fluid velocity. Krishna [19] discovered in a different analytical study that raising the importance of the Hall and ion slip parameters increases the fluid's velocity when it passes by a vertical plate that rotates indefinitely in an MHD field. Several recent research projects using various models have been carried out in this field [20,21,22,23,24,25].

Two important transport phenomena that are seen in multi-component systems are the Soret and Dufour effects. They stand for the mass and heat transfer that is out of balance due to temperature gradients and concentration gradients, respectively. The Soret effect is helpful in many areas. The Soret effect can be applied to separation procedures in the field of isotope separation, where different isotopes have different Soret coefficients. Procedures for isotope enrichment such as thermal diffusion columns or thermos gravitational columns may make use of these phenomena [26,27].

The Soret effect contributes to the movement of fuel and oxidizer species during combustion processes. Optimizing combustion processes, increasing efficiency, and lowering pollutant emissions, are helpful to understand the Soret effect. The Dufour effect, also known as thermal diffusion of heat, is a term used to describe how concentration gradients in a multi-component system induce heat to move. It defines the process where temperature gradients cause the mass to move, causing heat to transfer and chemical species to diffuse at the same time. In biological systems such as blood flow and tissue engineering, the Dufour effect plays a critical role. It affects the flow of heat and metabolites across tissues and plays a role in medical procedures like thermal ablation and drug delivery. Jawad et al. [28] investigate magnetohydrodynamic laminar flow on a vertical permeable surface in the context of Dufour and Soret implications. They find that an increase in the Prandtl number maximizes heat transfer. Mahdy [29] reviewed the heat characteristics of a Casson liquid caused by a stretching cylinder with the Soret and Dufour impacts. The study undertaken by Reddy et al. [30] examined the implications of radiation and Dufour consequences on the laminar motion of a rotating liquid that passes through a vertical plate. There have been recent attempts to inspect this subject [31,32,33,34,35,36,37,38]. Readers interested in solving differential equations using integral transforms can refer to the following sources: [41,41,43,44].

In this work, the effects of Soret, Dufour, and chemical processes are examined in relation to the flow of a fluid through a porous media that is experiencing unstable MHD laminar flow past a vertical plate that is spinning. The ND Solve command in MATHEMATICA was used to solve the dimensionless equations. The influence of several physical factors on temperature, velocity, and concentration profiles was visualized using numerical simulations. Furthermore, a comparison study with extant literature was conducted, which demonstrated a robust association between the present findings and prior research outcomes.

2. Mathematical formulation

Consider a rotating fluid that flows laminarly through a permeable plate in a conducting field of varying temperature and concentration. x-Axis is taken along the plate, which is in the vertical direction, considering the chemical reaction, radiation, and Dufour effects. The y-axis is considered normal to the

plate's surface. In a rigid body condition, both the plate and the liquid rotate through an unvarying angular velocity around the y-axis. At $t^* \le 0$, both the liquid and the plate were at rest, with uniform temperatures and concentrations T_{∞} & C_{∞} . The plate begins moving in the x-direction via uniform velocity. $u_0 a^* t^*$ at time $t^* > 0$. The temperature as well as concentration rise to $T_{\infty} + (T_w^* - T_{\infty}) \left(\frac{t^*}{t_0}\right)$ and $C_{\infty} + (C_w^* - C_{\infty}) \left(\frac{t^*}{t_0}\right)$ respectively. Later T_{∞} and C_{∞} are kept constant. Fig. 1 describes the physical interpretation of the above hypothesis.

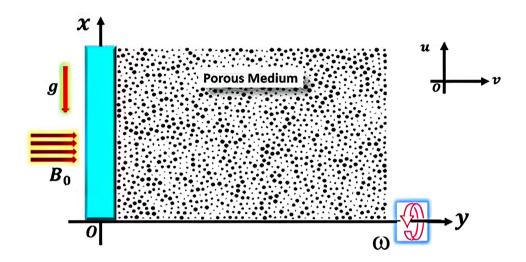


Figure 1: Physical model of the problem

The equations that determine the flow may be written as follows, taking these factors into account [25].

$$\frac{\partial u^{*}}{\partial t^{*}} + 2wv^{*} = v(1 + \frac{1}{\beta})\frac{\partial^{2}u^{*}}{\partial u^{*^{2}}} + g\beta_{T}\left(T^{*} - T_{\infty}\right) + g\beta_{c}\left(C^{*} - C_{\infty}\right) - \frac{\sigma B_{0}^{2}u^{*}}{\rho} - \frac{v}{k}u^{*} \tag{2.1}$$

$$\frac{\partial v^*}{\partial t^*} - 2wu^* = v(1 + \frac{1}{\beta}) \frac{\partial^2 V^*}{\partial y^{*2}} - \frac{\sigma B_0^2 v^*}{\rho} - \frac{v}{k} v^*$$

$$\tag{2.2}$$

$$\rho C_p \frac{\partial T^*}{\partial t^*} = k \frac{\partial^2 T^*}{\partial y^{*2}} + Q^* \left(T^* - T_\infty \right) - \frac{\partial q_r^*}{\partial y^*} + \frac{D_M k_T \rho}{C_s} \frac{\partial^2 C^*}{\partial y^{*2}}$$

$$\tag{2.3}$$

$$\frac{\partial C^*}{\partial t^*} = D \frac{\partial^2 C^*}{\partial y^{*2}} + \frac{D_M k_T}{T_M} \frac{\partial^2 T^*}{\partial y^{*2}} - Kr^* \left(C^* - C_\infty \right)$$
(2.4)

Associated initial & boundary conditions are [25],

$$\begin{cases} u^{*} = 0, \quad v^{*} = 0, \quad T^{*} = T_{\infty}, \quad C^{*} = C_{\infty} \text{For all} \quad t^{*}, y^{*} \leq 0 \\ u^{*} = u_{0}a^{*}t^{*}, \quad v^{*} = u_{0}a^{*}t^{*}, \quad T^{*} = T_{\infty} + (T_{w}^{*} - T_{\infty}) \left(\frac{t^{*}}{t_{0}}\right), \quad C^{*} = C_{\infty} + (C_{w}^{*} - C_{\infty}) \left(\frac{t^{*}}{t_{0}}\right) at \\ u^{*} = 0, \quad T^{*} = T_{\infty}, \quad C^{*} = C_{\infty} \text{ As} \qquad y \to \infty \end{cases}$$

$$(2.5)$$

Rosseland's estimate for radiative heat flux approximation:

$$q_r^* = -\frac{4\sigma^*}{3k^*} \frac{\partial T^{*4}}{\partial y^*} \tag{2.6}$$

Here k^* denotes the mean absorption term and σ^* denotes the Stefan-Boltzmann constant. The equation of T^{*4} is a linear function to keep the flow temperature variance as small as possible. As an impact, T^{*4} has been expanded utilizing the Taylor series about T^*_{∞} . By neglecting the higher-power components greater than the first degree, so:

$$T^4 \approx 4T_{\infty}^{*3}T - 3T_{\infty}^{*4}$$
 (2.7)

Using Eqs. (2.6) and (2.7), Eq. (2.3) becomes

$$\rho C_p \frac{\partial T^*}{\partial t^*} = k \frac{\partial^2 T^*}{\partial y^{*2}} + Q^* \left(T^* - T_\infty \right) + \frac{16T_\infty^{*3} \sigma^*}{3k^*} \frac{\partial^2 T^*}{\partial y^{*2}} + \frac{D_m k_T \rho}{C_w} \frac{\partial^2 C^*}{\partial y^{*2}}$$
(2.8)

The following are the non-dimensional quantities:

$$u = \frac{u^*}{u_0}, \quad v = \frac{v^*}{u_0}, \quad t = \frac{t^* u_0^2}{v}, \quad y = \frac{y^* u_0}{v}, \quad \theta = \frac{T^* - T_\infty}{T_w^* - T_\infty}, \quad C = \frac{C^* - C_\infty}{C_w^* - T_\infty}, \quad a = \frac{a^* v}{u_0^2}, l_1^2 = \frac{wv}{u^2}$$

$$Gr = \frac{vg\beta_T \left(T_w^* - T_\infty\right)}{u_0^3}, \quad Gm = \frac{vg\beta_c \left(C_w^* - C_\infty\right)}{u^3}, \quad M = \frac{\sigma B_0^2 v}{\rho u_0^2}, \quad K = \frac{K_1 U_0^2}{v^2}, \quad Pr = \frac{\rho v C_p}{k}, \quad Kr = \frac{Kr^* v}{u_0^2},$$

$$Q = \frac{Q^* v}{\rho C_p u_0^2}, \quad R = \frac{4\sigma^* T_\infty^{*3}}{3kk^*}, \quad S_c = \frac{v}{D}, \quad D_f = \frac{D_m K_T \left(C_w^* - C_\infty\right)}{v C_s C_p \left(T_w^* - T_\infty\right)}, \quad Sr = \frac{D_m k_T \left(T_w^* - T_\infty\right)}{v T_m \left(C_w^* - C_\infty\right)}$$

$$(2.9)$$

Equations (2.1), (2.2), (2.4), and (2.8) are recast as the following PDE's considering Eq. (2.9).

$$\frac{\partial u}{\partial t} + 2l_1^2 v = \left(1 + \frac{1}{\beta}\right) \frac{\partial^2 u}{\partial y^2} + Gr\theta + Gm \ C - Mu - \frac{1}{K}u \tag{2.10}$$

$$\frac{\partial v}{\partial t} - 2l_1^2 u = (1 + \frac{1}{\beta}) \frac{\partial^2 V}{\partial u^2} - Mv - \frac{1}{K} v \tag{2.11}$$

$$\frac{\partial \theta}{\partial t} = \frac{1}{Pr} \left(1 + \frac{4R}{3}\right) \frac{\partial^2 \theta}{\partial y^2} + Q\theta + Df \frac{\partial^2 C}{\partial y^2} \tag{2.12}$$

$$\frac{\partial C}{\partial t} = \frac{1}{Sc} \frac{\partial^2 C}{\partial y^2} - KrC + Sr \frac{\partial^2 \theta}{\partial y^2}$$
 (2.13)

The initial boundary conditions (BCs) are:

$$u=0, \quad v=0, \quad \theta=0, \quad C=0, \quad \forall y, \, t \leq 0 \quad t>0;$$

$$u=e^{at}, \quad v=e^{at}. \quad \theta=t, \quad C=t \quad \text{at} \quad y=0,$$

$$u=0, \quad v=0, \quad \theta^*=0, \quad C=0, \quad as \quad y\to\infty \qquad (2.14)$$

3. Results and Discussion

To extract the physical significance of the problem depicted in Figures 2–13, a simulation for transient MHD rotating laminar flow through a vertical plate in a permeable material by Soret, Dufour, and chemical reactions has been constructed using numerous dissimilar non-dimensional flow parameters. Many real-world applications, including geosciences and chemical engineering, include the Soret and Dufour effects. Analysis of the Grid Independence is presented in Table 1, 2 and 3 for different mesh lengths which demonstrates the consistency of the numerical approach. In the progression of this investigation, the following default parameters have been selected:

$$M=1.0, Df=1.0, K=0.5, Q=0.5, t=0.2, a=2, Sc=0.22, Gr=5.0,$$

 $Sr=1.0, Gc=5, R=0.5, Pr=0.71 \& Kr=0.5.$

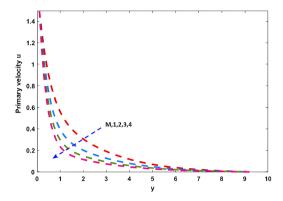


Figure 2: Primary velocity profiles on M

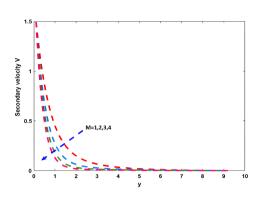


Figure 3: Secondary velocity profiles on M

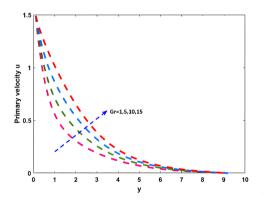


Figure 4: Primary velocity profiles on Gr

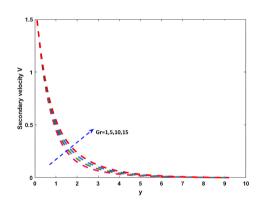


Figure 5: Secondary velocity profiles on Gr.

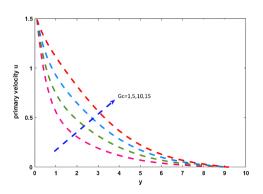


Figure 6: Primary velocity profiles on Gc

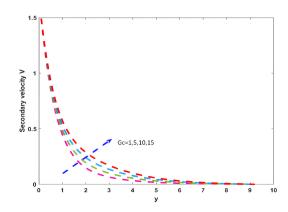


Figure 7: Secondary velocity profiles on Gc.

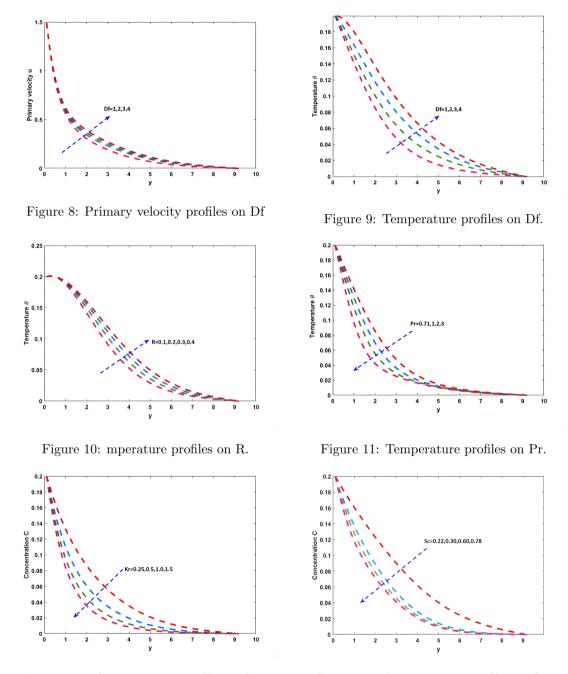


Figure 12: Concentration profiles on Kr.

Figure 13: Concentration profiles on Sc.

Figures 2 and 3 illustrate the impact of M on the velocity profile. As the values of M rise, the flow velocity progressively decreases. The Lorentz force, a kind of resistance, was responsible for this phenomenon because it was produced by the induced magnetic field created by the liquid movement. Consequently, both the heaviness of the boundary layer and the motion of the fluid will decrease monotonically. Figs. 4 and 5 portray the impact of Grashof number (Gr) on the velocity profile. Gr is a dimensionless quantity that shows how important buoyancy forces are related to viscous forces in the flow of a stream. It is frequently employed in the study of natural convection, where buoyancy effects resulting from temperature differences drive fluid motion. The Grashof number influences the velocity profile of a fluid enduring natural convection significantly. As the Grashof number goes up, buoyancy forces get stronger, but viscous forces don't, so the velocity curves go up. The behavior of modified Grashof number Gc on

the velocity profile is seen in Figs. 6 and 7. The modified Grashof number, a dimensionless quantity, illustrates the relative impact of concentration buoyant forces and viscous forces in stream flow. The buoyant forces get greater while the viscous forces remain constant when the concentration Grashof number Gc rises, increasing the velocity curves.

The effect of the Dufour number (Df) on the primary temperature and velocity is seen in Figures 8 and 9. The Dufour number (Df) is a dimensionless metric that indicates the mass diffusion to heat diffusion ratio in fluid mixtures. In conditions with temperature and concentration gradients, such as chemical reactions and combustion, it is essential for mass and heat transfer mechanisms. By influencing the temperature and concentration distributions within a fluid, the Df indirectly influences the primary velocity. Temperature gradients change when heat diffusion overtakes mass diffusion at increasing Dufour numbers. These fluctuations may result in buoyancy effects that change the density distribution and may have an impact on natural convection flow patterns. The dependency of temperature profiles θ on the radiation parameter R is shown in Figure 10. The radiative heat flux deviation rises with a drop in the mean absorption coefficient, which raises the temperature of the liquid near the surface and increases the rate of radiative heat transfer. As a result, for greater radiation levels, the thermal boundary layer's thickness and temperature profile also rise. The temperature distribution for a range of realistic Prandtl values is displayed in Figure 11. These numbers are notable since oxygen, air, ammonia, and carbon disulfide are all physically identical. The temperature drops as a result of the thermal boundary layer expanding and thermal conductivity decreasing as the Prandtl number Pr rises.

The consequence of chemical reaction parameters on concentration profiles in a chemical reaction system can be quite significant. Fig. 12 illustrates how Kr modifies the molecular concentration profiles. It demonstrates how the concentration of diffusing species quickly falls as Kr increases. The concentration of the diffusing species falls during the fast reaction, as seen above. Concentration distributions for plausible approximations of the Schmidt number are depicted in Fig. 13. The physical similarity between hydrogen, ammonia, oxygen, and water makes these values noteworthy. The Schmidt number denoted as Sc, is a measure of momentum diffusivity to mass diffusivity. Larger values of Sc are associated with lower molecular diffusivity and slower species diffusion in a fluid. These outcomes in a dramatic reduction in the heaviness of the concentration boundary layer as Sc rises.

Skin friction, Nusselt number, and Sherwood number:

Skin friction:
$$\tau = -\left(\frac{\partial u}{\partial y}\right)_{y=0}$$
:

Table 1: Numerical outcomes of the skin friction (τ)

K	Gm	M	Df	Kr	Gr	Sc	Sr	au
0.5	5	0.5	1.0	0.5	1	0.22	1	0.018631
1.0								0.014160
1.5								0.012502
2.0								0.011651
	5							0.016919
	10							0.015209
	15							0.013501
		1						0.018632
		1.5						0.020562
		2						0.022339

Nusselt Number: $Nu = \left(\frac{\partial \theta}{\partial y}\right)_{y=0}$

Pr	R	Q	Gr	Df	M	Kr	K	Nu
0.71	0.5	0.5	5.0	1.0	1.0	0.5	0.5	0.000101
1.00								0.000120
5.00								0.000241
	1.0							0.000069
	1.5							0.000048
	2.0							0.000019
		1.0						0.000846
		1.5						0.001958
		2.0						0.003688

Table 2: Numerical outcomes of Nusselt number Nu

Sherwood number values: $Sh = \left(\frac{\partial C}{\partial y}\right)_{y=0}$

Table 3: Numerical outcomes of Sherwood number values Sh

Sc	Kr	Gm	Df	M	Sr	K	Sh
0.22	0.5	0.5	1.0	1.0	1.0	0.5	-0.000762
0.30							-0.001721
0.60							-0.002581
0.78							-0.003522

4. Conclusions

In a transient magnetohydrodynamic (MHD) laminar flow, this study investigated the effects of Soret, Dufour, and chemical processes on the fluid dynamics within a porous media revolving around a vertical plate. The governing equations were numerically solved using the ND Solve technique. After that, numerical simulations were employed to show how different physical factors affected the profiles of temperature, velocity, and concentration.

- 1. As the magnitude of the magnetic parameter M expands, the velocity profiles exhibit a decreasing trend.
- 2. Enhancing the values of the radiation factor causes an upsurge in the temperature.
- 3. The concentration profiles with respect to higher Sr values are improved.
- 4. Enhancing the values of permeability causes a reduction in skin friction.
- 5. Improving the estimations of the heat absorption factor causes again in the Nusselt number values.

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